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(54) Gelling compositions useful for oil field applications

Gelierzusammensetzungen zur Verwendung in Ölfeldern

Compositions gélifiantes utilisables dans les gisements petrolifères

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EP 0 604 988 B1

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DescriptionField of the Invention

[0001] The present invention relates to a gelling composition and application therefor in oil field operations.

Background of the Invention

[0002] It is well known to those skilled in the art that gelled or cross linked water-soluble polymers are useful in enhanced oil recovery and other oil field operations. They have been used to alter the permeability of underground formations in order to enhance the effectiveness of water flooding operations. Generally, polymers along with an appropriate cross linking system are injected in an aqueous solution into the formation. The polymers then permeate into and gel in the regions having the highest water permeability.

[0003] Because of environmental concerns as well as cost for disposing of a produced brine which is defined as the brine co-produced with oil and gas, it is desirable to utilize the produced brine as the aqueous solution used for the polymers and appropriate cross linking system described above. Use of produced brines eliminates not only the cost associated with acquiring and pre-treating fresh water for use as the aqueous solution but also the disposal cost for the produced brine. Most produced brines are known to be hard brines, i.e., those having a salinity of greater than 2% total dissolved solids, basically inorganic salts. Chromium(III) carboxylates such as, for example, chromium acetate are the only known crosslinkers which can be used to produce stable gels in produced brines for near-wellbore treatment. See for example R.D. Sydansk, Acrylamide-Polymer/Chromium(III)-Carboxylate Gels for Near Wellbore Matrix Treatments, Proceedings SPE/DOE Seventh Symposium on Enhanced Oil Recovery (1990). Although a chromium(III) salt is not as toxic as a chromium(VI) salt, it is not an environmentally desirable compound and its use may require additional costs to assure the integrity of the injection wells to avoid contamination of ground water sources.

[0004] There is, therefore, a need to develop a more environmentally suitable gelling composition that can form stable gels in produced brines for near-wellbore as well as in-depth treatments. It would also be a significant contribution to the art if a gelling composition does not crosslink too fast (i.e., gel times longer than 2 hours) so that individual components of the gelling composition can be injected simultaneously into the wells.

Summary of the Invention

[0005] An object of the invention is to provide a gelling composition comprising produced brines having a high salinity. Another object of the invention is to provide a gelling composition that is environmentally suitable for use in oil field operations. A further object of the invention is to provide a gelling composition that delays gelation process so that all components of the gelling compositions can be injected simultaneously. Still another object of the invention is to provide a process for near-wellbore treatment employing a gelling composition that is environmentally suitable for oil field operations. An advantage of the invention is the delayed gelation of the composition so that, for near-wellbore treatment, the components of the composition can be simultaneously injected. Another advantage of the invention is the use of high salinity produced brines to eliminate the necessity of treating or disposing of the brines. Other objects, features, and advantages will become more apparent as the invention is more fully disclosed hereinbelow.

[0006] According to an embodiment of the invention, a composition as defined in claim 11 is provided which comprises a produced brine, a water-soluble polymer, a crosslinker, and a complexing ligand.

[0007] According to another embodiment of the invention, a process for wellbore treatment is provided as defined in claim 1.

Detailed Description of the Invention

[0008] According to the invention, a composition as defined in claim 11 that is useful for near-wellbore treatment in oil field operations comprises a produced brine, a water-soluble polymer, a crosslinker, and a complexing ligand. The near-wellbore treatment includes, but is not limited to, water shutoff, gas shutoff, and zone abandonment.

[0009] The produced brine employed in the composition of the invention is defined as the brine co-produced with oil or gas, or both, which generally is a hard brine, i.e., containing at least 1,000 ppm of Ca^{+2} , Ba^{+2} , Mg^{+2} , or Sr^{+2} , or combinations thereof. It generally contains high salinity of from 1% to 30% total dissolved solids. The composition of the invention also gels well in produced brines having a salinity of from 3% to 27%. To delay the rate of gelation so that the components of the composition can be injected at the same time without plugging up the injection or producing wells, a produced brine having a salinity of from 4% to 25% generally produces better results.

[0010] Polymers suitable for use in this invention are those capable of gelling in the presence of polyvalent metal ion crosslinking agents. Polymers suitable for use in this invention, i.e., those capable of gelling in the presence of

crosslinking agents within a gelation pH range, include biopolysaccharides, cellulose ethers, and acrylamide-based polymers.

[0011] Suitable cellulose ethers are disclosed in U.S. pat. no. 3,727,688. Particularly preferred cellulose ethers include carboxymethylhydroxyethyl cellulose (CMHEC) and carboxymethyl cellulose (CMC).

[0012] Suitable biopolysaccharides are disclosed in U.S. Pat. No. 4,068,714. Particularly preferred is polysaccharide B-1459 and xanthan gums which are biopolysaccharides produced by the action of *Xanthomonas campestris* bacteria. This biopolysaccharide is commercially available in various grades under the tradename Kelzan® (Kelco Company, Los Angeles, Calif.) and Flocon 4800 (Pfizer, Groton, CT).

[0013] Suitable acrylamide-containing polymers which also contain small amounts of pendant carboxylate (acrylate) groups are disclosed in U.S. Pat. No. 3,749,172. As used herein, the term "small amounts" refers to about 0.5 to 5 mole percent. Particularly preferred are the so-called partially hydrolyzed polyacrylamides possessing pendant carboxylate groups through which crosslinking can take place. Thermally stable polymers of acrylamide, such as copolymers of N-vinyl-2-pyrrolidone and acrylamide terpolymers of sodium-2-acrylamido-2-methylpropanesulfonate, acrylamide and N-vinyl-2-pyrrolidone, and copolymers of sodium-2-acrylamido-2-methyl-1-propanesulfonate and acrylamide, are particularly preferred for applications in high salinity environments at elevated temperatures. Selected terpolymers also are useful in the present process, such as terpolymers derived from acrylamide and N-vinyl-2-pyrrolidone comonomers with lesser amounts of monomers such as vinyl acetate, vinylpyridine, styrene, methyl methacrylate, and other polymers containing acrylate groups.

[0014] Other miscellaneous polymers suitable for use in the present invention include partially hydrolyzed polyacrylonitrile, polystyrene sulfonate, lignosulfonates, methylolated polyacrylamides, and the like.

[0015] Presently preferred are CMC, xanthan gum, and the acrylamide based polymers, particularly the partially hydrolyzed polyacrylamides, polymers containing acrylamide, ammonium or alkali salt of acrylic acid, and polymers containing ammonium or alkali salt of acrylic acid, N-vinyl-2-pyrrolidone, and sodium-2-acrylamido-2-methylpropanesulfonate.

[0016] The crosslinker useful in the present invention is a metal compound selected from the group consisting of a complexed zirconium compound, a complexed titanium compound, and mixtures thereof. Examples of suitable crosslinker include, but are not limited to, ammonium zirconium fluoride, zirconium 2-ethylhexanoate, zirconium acetate, zirconium neodecanoate, zirconium acetylacetonate, tetrakis(triethanolamine)zirconate, zirconium carbonate, ammonium zirconium carbonate, zirconyl ammonium carbonate, titanium acetylacetonate, titanium ethylacetoacetate, zirconium lactate, titanium triethanolamine, ammonium titanium lactate, and combinations thereof. These compounds are commercially available.

[0017] The complexing ligand used in the composition of the present invention to retard the rate of gelation is malonic acid, ammonium, potassium or sodium malonate, and mixtures thereof.

[0018] The composition of the invention can be prepared by mixing the individual components together employing conventionally well-known mixing means. The order of adding individual components does not change the characteristics of the composition.

[0019] The concentration or amount of the water-soluble polymer in the aqueous solution can range widely and be as suitable and convenient for the various polymers, and for the degree of gelation needed for particular reservoirs. Generally, the concentration of polymer in its aqueous solution is made up to a convenient strength of 100 to 20,000 ppm, preferably 200 to 7,000 ppm.

[0020] Any suitable procedures for preparing the aqueous admixtures of the crosslinkable polymer can be used. Some of the polymers may require particular mixing conditions, such as slow addition of finely powdered polymer into the vortex of stirred brine, alcohol pretreatment, protection from air (oxygen), preparation of stock solutions from fresh rather than salt water, or the like, as is known for such polymers.

[0021] The concentration of crosslinker in the composition depends largely on the concentrations of polymer in the composition. Lower concentrations of polymer, e.g., require lower concentrations of crosslinker. Further, it has been found that for a given concentration of polymer, increasing the concentration of crosslinker generally substantially increases the rate of gelation. The concentration of crosslinker in the injected slug varies generally over the broad range of 25 ppm to 5,000 ppm, preferably over the range of 100 ppm to 2,000 ppm based on Zr or Ti concentration.

[0022] The concentration of the complexing ligand in the composition also depends on the concentrations of the water-soluble polymer in the composition and on the desired rate of gelation. Generally, the faster the gelation rate, the lower concentration of the complexing ligand is required. Generally, the concentration of the complexing ligand varies broadly in the range of 25 ppm to 5,000 ppm, preferably in the range of 50 ppm to 3,000 ppm, and most preferably in the range of 100 ppm to 2,000 ppm.

[0023] According to further embodiment of the invention, a process for near-wellbore treatment in an oil field operation falling under claim 1 comprises simultaneously injecting a produced brine, a water-soluble polymer, a crosslinker and a complexing ligand into an injection well. The definition and scope of the produced brine, water-soluble polymer, crosslinker and complexing ligand are the same as those described in the composition of the invention. The water-

soluble polymer, crosslinker and complexing ligand can also be injected sequentially without special order of injection, as long as they are first dissolved in the produced brine. In order to delay the gelation, however, it is preferred that the complexing ligand and crosslinker be mixed together in the produced brine prior to injecting.

[0024] The use of gelled polymers to alter the water permeability of underground formations is well known to those skilled in the art. Generally, an aqueous solution containing the polymer and a crosslinker is pumped into the formation so that it can diffuse into the more water swept portions of the formation and alter water permeability by gelling therein.

[0025] The present invention can be used in a similar manner. An aqueous solution of the composition of the present invention can be pumped into the formation so that it alters the water permeability of the formation in a similar manner when gelation takes place. The aqueous solution containing the water soluble polymer and a zirconium or titanium crosslinker solution in the presence or absence of the complexing ligand can be pumped into the formation in one slug, or alternatively the components may be sequentially injected in a manner to provide an appropriate concentration in the formation.

[0026] The nature of the underground formation treated is not critical to the practice of the present invention. The described gelable composition can be injected into a formation having a temperature range of from 70°F to 300°F when the polymer used is a copolymer having the repeating units derived from at least one monomer selected from the group consisting of N-vinyl-2-pyrrolidone, sodium-2-acrylamido-2-methylpropane sulfonate, acrylamide, an alkali salt of acrylic acid and combinations thereof; or a temperature in the range of from 70°F to 200°F for partially hydrolyzed polyacrylamide, xanthan gum, CMC, or CMHEC, preferably 80°F to 180°F, and most preferably 90°F to 170°F.

[0027] Examples provided hereinbelow are intended to assist one skilled in the art to further understand the invention and should not be considered limitative.

Example I

[0028] The purpose of this example is to illustrate the gelation of a composition comprising a water-soluble polymer, a crosslinker and a brine, and to use this example as a control.

[0029] Polyacrylamide solutions (0.5%) were prepared by mixing sufficient amount of the polymer in a synthetic brine having 1.1%, total dissolved solids (TDS; 1% NaCl and 0.1% CaCl₂), 11% TDS (10% NaCl and 1% CaCl₂), and 22% TDS (20% NaCl and 2% CaCl₂). Then 20 ml samples of each polymer solution were placed in three vials. Each vial was then charged with tetrakis(triethanolamine)zirconate. The vials were placed upright in test tube racks and then placed in ovens heated to and held at 120°F. Periodically, the ampules were removed from the oven and the mechanical strength of the gels was determined.

[0030] As crosslinking developed, small microgels of granules began to appear, i.e., a very slight gel formed. Continued growth of the microgels to globule occurred next, referred to as slight gel. Larger gel masses next appeared, referred to as partial gel, followed by the development of stronger gels with measurable tongue lengths. The tongue lengths were measured by placing each vial horizontally allowing the hot gelling composition to flow to its equilibrium position and then measuring the length of the tongue formed. As gelation progressed with time, stronger gels and shorter tongue lengths were developed. The gel strength is expressed mathematically as

$$\text{Percent Gel Strength} = (\text{AL} - \text{TL}) \times 100 / \text{AL}$$

where AL equals ampule length (in centimeters), and TL equals the tongue length of the gel measured in centimeters from the point at which the gel contacts the entire circumference of the tube to the farthest point to which the gel has spread. Thus the strongest gels would have a gel strength of 100% and the weakest gels would have a gel strength of 0. The gel strength results are shown in Table I.

Table I

Gelation of Polyacrylamide ^a in Brines with 250 ppm Zirconium (Zirtech TE ^b) at 120°F					
In 1.1% Brine		In 11% Brine		In 22% Brine	
Aging Time (days)	Gel Strength (%)	Aging Time (days)	Gel Strength (%)	Aging Time (days)	Gel Strength (%)
0.06	0.00	0.07	64.4	0.06	84.0
0.15	64.9	0.17	70.7	0.16	84.0

^aPolymer used was Polydia 1041 (% hydrolysis=3-6; inherent viscosity = 18 dL/g) obtained from Nitto Chemical Industry Co., Tokyo, Japan.

^bZirtech TE is a triethanolamine complex of Zirconium obtained from Benchmark Research and Technology, Inc., Midland, Texas.

Table I (continued)

Gelation of Polyacrylamide ^a in Brines with 250 ppm Zirconium (Zirtech TE ^b) at 120°F					
In 1.1% Brine		In 11% Brine		In 22% Brine	
Aging Time (days)	Gel Strength (%)	Aging Time (days)	Gel Strength (%)	Aging Time (days)	Gel Strength (%)
0.81	71.6	0.84	77.3	0.84	86.7
2.90	78.7	3.90	80.4	3.90	87.1
4.90	81.3	5.90	83.6	5.80	87.6
7.00	81.3	7.90	84.4	7.80	88.4
11.30	83.6	14.90	85.3	14.90	90.7
18.20	84.4	22.00	86.2	21.90	88.9
25.20	84.0	29.00	87.1	28.90	91.1
32.00	86.2	36.00	87.1	36.00	91.1
39.00	86.2	43.00	85.8	43.00	91.6
46.00	87.6	77.00	87.1	70.00	90.7
53.00	88.4	152.00	85.8	146.00	77.8
87.00	88.4	246.00	82.7	193.00	77.8
162.00	88.4				
256.00	88.4				

^aPolymer used was Polydia 1041 (% hydrolysis=3-6; inherent viscosity = 18 dL/g) obtained from Nilto Chemical Industry Co., Tokyo, Japan.

^bZirtech TE is a triethanolamine complex of Zirconium obtained from Benchmark Research and Technology, Inc., Midland, Texas.

[0031] The results shown in Table I indicate that increasing the salinity of the brines from 1.1% to 22% significantly increased the gelation rate. For example, aging for 1.4 hours (0.06 day), the gel strength in 1.1% brine was 0.0. The gel strength in 22% brine, for same aging period, increased to 84%. However, upon prolonged incubation, the gels formed in lower salinity brine appears to have stronger gels than those formed in higher salinity brines. For example, upon gelling for 256 days in 1.1% brine, the gel strength was 88.4%. On the other hand, upon gelling for 193 days in 22% brine, the gel strength was only 77.8%.

Example II

[0032] This example illustrates the gelation of water-soluble polymer with a complexed zirconium compound in a produced brine.

[0033] The runs were carried out the same as those described in Example I with the exception that the brine used is a produced brine obtained from Tank Battery 41 of North Burbank Unit Oil Field, Shidler, Oklahoma. The produced brine has a TDS of 5%. Gel strength of the gels aged at 48.9°C, 65.6°C and 79.4°C (120°F, 150°F and 175°F) is shown in Table II.

Table II

Gelation of Polyacrylamide in a Produced Brine with Zirtech TE (250 ppm Zr) at 120°F, 150°F and 175°F			
Aging Time (days)	Gel Strength (%)		
	120°F	150°F	175°F
0.06	0.0	65.8	84.9
0.17	0.0	74.7	92.4
0.83	67.6	83.6	94.2
1.20	72.4	85.3	95.1
1.90	74.2	87.1	96.0
2.80	77.8	88.4	95.6
7.80	80.4	89.8	96.4
20.00	83.6	91.6	96.9
26.90	84.9	92.4	97.3

Table II (continued)

Gelation of Polyacrylamide in a Produced Brine with Zirtech TE (250 ppm Zr) at 120°F, 150°F and 175°F			
Aging Time (days)	Gel Strength (%)		
	120°F	150°F	175°F
34.00	84.9	92.0	96.9
49.00	86.2	93.8	91.1
66.00	87.6	93.3	86.2
97.00	89.3	93.8	Syneresis
125.00	88.4	93.8	Syneresis

[0034] Table II shows that the lower the aging temperature, the slower the gelation rate. For instance, no gel was observed at 120°F until after the gelling composition had been aged for more than 4.1 hours (0.17 day). It gelled, however, within 1.4 hours of aging at 150°F as well as at 175°F. Table II further indicates that the gelation rate at higher temperature, i.e. 150°F to 175°F, needed to be delayed so that the components of the gelling composition can be simultaneously injected into an oil well.

Example III

[0035] This example shows the effect of crosslinker pH on the gelation of polyacrylamide in a produced brine.

[0036] The runs were carried out the same as described in Example II except that the crosslinker pH was adjusted to the values shown in Table III using a 20-25% NaOH solution. The aging was done at 120°F only. The results are shown in Table III.

Table III

Effect of pH on Gelation Polyacrylamide in a Produced Brine with Zirtech TE (250 ppm Zr) at 120°F			
Aging Time (days)	Gel Strength (%) at pH		
	6.7	7.34	8.07
0.05	58.7	0.0	0.0
0.17	69.8	0.0	0.0
0.83	78.2	59.7	0.0
1.80	78.7	60.0	0.0
4.10	79.6	59.6	0.0
33.00	80.0	71.1	0.0
70.00	80.9		

[0037] Table III indicates that for prolonged aging at 120°F a pH higher than 7.34 was not suitable. Table III further indicates that the gelation rate can also be adjusted by adjusting the pH of crosslinker solution.

Example IV

[0038] This example demonstrates that the gelation rate of a gelling composition comprising polymer and a complexed zirconium compound in a produced brine can be reduced by adding a complexing ligand to the gelling composition.

[0039] All runs shown in Table IV below were carried out the same as those described in Example II except that malonic acid was added to the composition (to a final concentration of 400 ppm) before aging at 120°F. Results are shown in Table IV.

Table IV

Effect of Malonic Acid on Gelation of Polyacrylamide in a Produced Brine with Zirtech TE at 120°F			
Aging Time (days)	Gel Strength (%)		
	No Acid	With Acid	
0.05	64.4	0.0	
0.12	75.6	71.1	
0.19	78.2	77.8	
0.84	81.3	84.9	
4.10	83.6	88.0	
10.10	84.4	90.2	
39.00	85.3	92.9	
76.00	87.1	94.7	

[0040] The results shown in Table IV demonstrate that the gelation rate of the composition was developed. In the presence of 400 ppm malonic acid, the gelling composition did not form gels until after being aged for at least 1.2 hours (0.05 day).

Example V

[0041] This example illustrates that sodium acetate is not an effective complexing ligand for delaying gelation of the invention composition.

[0042] The runs were carried out the same as those described in Example IV except that sodium acetate (Na-Acet) was used in place of malonic acid, zirconium lactate was used as the crosslinker and the produced brine used was obtained from Tank Battery 57 from North Burbank Unit and had 10% TDS. The results are shown in Table V.

Table V

Effect of Sodium Acetate on Gelation of Polyacrylamide in a Produced Brine with Zirtech TE (250 ppm Zr) at 120°F			
Aging Time (days)	Gel Strength (%)		
	0 ppm Na-Acet	300 ppm Na-Acet	
0.04	79.5	75.1	
0.08	82.7	81.3	
0.13	84.9	84.0	
0.17	84.9	84.0	
0.87	88.0	88.9	
4.80	91.1	90.7	
5.90	90.7	90.7	
10.90	90.2	89.8	
18.90	92.0	91.1	
28.10	92.0	90.7	

[0043] Table V shows that gelling composition gelled almost instantly upon aging, even in the presence of 978 ppm sodium acetate in the composition.

[0044] The results shown in the above examples clearly demonstrate that the present invention is well adapted to carry out the objects and attain the ends and advantages mentioned as well as those inherent therein.

Claims

1. A process for wellbore treatment comprising injecting a composition comprising a produced brine which is co-produced with oil and/or gas, a water-soluble polymer, and a crosslinker being selected from complexed zirconium compounds, complexed titanium compounds, and combinations thereof, characterized in that the composition

further comprises a complexing ligand being selected from malonic acid, ammonium malonate, sodium malonate, potassium malonate, and mixtures thereof.

2. The process of claim 1 wherein said wellbore treatment comprises water shutoff, gas shutoff, and zone abandonment.
3. The process of claim 1 or 2 wherein said water-soluble polymer is selected from biopolysaccharides, cellulose ethers, acrylamide-containing polymers having from 0.5 to 5 mole percent of carboxylate groups, and combinations thereof; in particular wherein said water-soluble polymer is an acrylamide-containing polymer or a partially hydrolyzed polyacrylamide.
4. The process of any of the preceding claims wherein said crosslinker is selected from ammonium zirconium fluoride, zirconium 2-ethylhexanoate, zirconium acetate, zirconium neodecanoate, zirconium acetylacetonate, tetrakis(triethanolamine)zirconate, zirconium carbonate, ammonium zirconium carbonate, zirconyl ammonium carbonate, titanium acetylacetonate, titanium ethylacetoacetate, zirconium lactate, titanium triethanolamine, ammonium titanium lactate and combinations thereof.
5. The process of any of the preceding claims wherein the salinity of said produced brine is in the range of 1 to 30 %, preferably from 3 to 27 %, and most preferably from 4 to 25 %, each based on total dissolved solids.
6. The process of any of the preceding claims wherein the concentration of said water-soluble polymer in said produced brine is in the range of 100 to 20,000 ppm, preferably in the range of 200 to 7,000 ppm.
7. The process of any of the preceding claims wherein the concentration of said crosslinker in said produced brine is in the range of from 25 to 5,000 ppm, preferably in the range of 100 to 2,000 ppm.
8. The process of any of the preceding claims wherein the concentration of said complexing ligand in said produced brine is in the range of 25 to 5,000 ppm, preferably in the range of 200 to 2,000 ppm.
9. The process of any of the preceding claims wherein said composition is injected into an oil or gas well in a temperature range of 26.7 to 93 °C, preferably 37.8 to 77 °C.
10. The process of claim 1 wherein said composition is injected into an oil or gas well in a temperature range of 21, 1 to 149 °C, preferably 66 to 121 °C, and wherein said polymer is a copolymer having the repeating units derived from monomers selected from acrylamide, N-vinyl-2-pyrrolidone, sodium 2-acrylamido-2-methylpropane sulfonate, acrylic acid, and alkali salt of acrylic acid, and combinations thereof.
11. A composition suitable for wellbore treatment comprising a produced brine, a water-soluble polymer, a crosslinker, and a complexing ligand, said components being defined as in any of claims 1, 3 to 9, and 10.

Patentansprüche

1. Verfahren zur Bohrloch-Behandlung, umfassend die Injektion einer Zusammensetzung, die eine geförderte Salzlösung, die bei der Förderung von Öl und/oder Gas mit anfällt, ein wasserlösliches Polymeres und ein Vernetzungsmittel, ausgewählt aus Zirkonium-Komplexverbindungen, Titan-Komplexverbindungen, und aus Kombinationen hiervon, enthält, dadurch gekennzeichnet, daß die Zusammensetzung außerdem einen komplexierenden Liganden enthält, der ausgewählt ist aus Malonsäure, Ammoniummalonat, Natriummalonat, Kaliummalonat, und aus Gemischen hiervon.
2. Verfahren nach Anspruch 1, wobei die Bohrloch-Behandlung das Absperren von Wasser, das Absperren von Gas und die Zonenaufgabe umfaßt.
3. Verfahren nach Anspruch 1 oder 2, wobei das wasserlösliche Polymere ausgewählt ist aus Biopolysacchariden, Celluloseethern, Acrylamid-haltigen Polymeren mit 0,5 bis 5 Mol-% Carboxylatgruppen, und aus Kombinationen hiervon, wobei das wasserlösliche Polymere insbesondere ein Acrylamid-haltiges Polymeres oder ein teilweise hydrolysiertes Polyacrylamid ist.

4. Verfahren nach einem der vorhergehenden Ansprüche, wobei das Vernetzungsmittel ausgewählt ist aus Ammoniumzirkoniumfluorid, Zirkonium-2-ethylhexanoat, Zirkoniumacetat, Zirkoniumneodecanoat, Zirkoniumacetylacetonat, Tetrakis-(triethanolamin)zirconat, Zirkoniumcarbonat, Ammoniumzirkoniumcarbonat, Zirkonylammoniumcarbonat, Titanacetylacetonat, Titanethylacetoacetat, Zirkoniumlactat, Titantriethanolamin, Ammoniumtitanlactat, und aus Kombinationen hiervon.
5. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Salzgehalt der geförderten Salzlösung im Bereich von 1 bis 30 %, vorzugsweise 3 bis 27 % und besonders bevorzugt 4 bis 25 % liegt, jeweils bezogen auf gesamte gelöste Feststoffe.
6. Verfahren nach einem der vorhergehenden Ansprüche, wobei die Konzentration des wasserlöslichen Polymeren in der geförderten Salzlösung im Bereich von 100 bis 20 000 ppm, vorzugsweise im Bereich von 200 bis 7 000 ppm liegt.
7. Verfahren nach einem der vorhergehenden Ansprüche, wobei die Konzentration des Vernetzungsmittels in der geförderten Salzlösung im Bereich von 25 bis 5 000 ppm, vorzugsweise im Bereich von 100 bis 2 000 ppm liegt.
8. Verfahren nach einem der vorhergehenden Ansprüche, wobei die Konzentration des komplexierenden Liganden in der geförderten Salzlösung im Bereich von 25 bis 5 000 ppm, vorzugsweise im Bereich von 100 bis 2 000 ppm liegt.
9. Verfahren nach einem der vorhergehenden Ansprüche, wobei die Zusammensetzung in ein Öl- oder Gasbohrloch in einem Temperaturbereich von 26,7 bis 93 °C, vorzugsweise 37,8 bis 77 °C, injiziert wird.
10. Verfahren nach Anspruch 1, wobei die Zusammensetzung in ein Öl- oder Gasbohrloch in einem Temperaturbereich von 21,1 bis 149 °C, vorzugsweise 66 bis 121 °C, injiziert wird, und wobei das Polymere ein Copolymeres mit den Grundbausteinen ist, die sich von Monomeren ableiten, die ausgewählt sind aus Acrylamid, N-Vinyl-2-pyrrolidon, Natrium-2-acrylamido-2-methylpropansulfonat, Acrylsäure und einem Alkalisalz der Acrylsäure, und aus Kombinationen hiervon.
11. Zusammensetzung, die zur Bohrloch-Behandlung geeignet ist und eine geförderte Salzlösung, ein wasserlösliches Polymeres, ein Vernetzungsmittel und einen komplexierenden Liganden enthält, wobei die Komponenten in einem der Ansprüche 1, 3 bis 9 und 10 definiert sind.

Revendications

1. Un procédé pour le traitement de puits de forage consistant à injecter une composition comprenant une saumure produite qui est co-produite avec de l'huile et/ou du gaz, un polymère soluble dans l'eau et un agent de réticulation choisi parmi les composés de zirconium complexés, les composés de titane complexés et leurs combinaisons, caractérisé en ce que la composition comprend, en outre, un ligand complexant choisi parmi l'acide malonique, le malonate d'ammonium, le malonate de sodium, le malonate de potassium et leurs mélanges.
2. Le procédé selon la revendication 1, dans lequel ledit traitement de puits de forage comprend une coupure d'eau, une coupure de gaz et un abandon de zone.
3. Le procédé selon la revendication 1 ou 2, dans lequel ledit polymère soluble dans l'eau est choisi parmi les biopolysaccharides, les éthers de cellulose, les polymères renfermant de l'acrylamide ayant de 0,5 à 5 % en moles de groupes carboxylate et leurs combinaisons, en particulier dans lequel ledit polymère soluble dans l'eau est un polymère contenant de l'acrylamide ou un polyacrylamide partiellement hydrolysé.
4. Le procédé selon l'une quelconque des revendications précédentes, dans lequel ledit agent de réticulation est choisi parmi le fluorure de zirconium-ammonium, le 2-éthylhexanoate de zirconium, l'acétate de zirconium, le néo-décanoate de zirconium, l'acétylacétonate de zirconium, le zirconate de tétrakis(triéthanolamine), le carbonate de zirconium, le carbonate de zirconium-ammonium, le carbonate de zirconyl-ammonium, l'acétylacétonate de titane, l'éthylacétoacétate de titane, le lactate de zirconium, le triéthanolamine-titane, le lactate de titane-ammonium et leurs combinaisons.

5. Le procédé selon l'une quelconque des revendications précédentes, dans lequel la salinité de ladite saumure produite se situe dans la gamme de 1 à 30%, de préférence de 3 à 27% et mieux encore de 4 à 25%, chacun étant calculé sur les solides dissous totaux.

5 6. Le procédé selon l'une quelconque des revendications précédentes, dans lequel la concentration dudit polymère soluble dans l'eau dans ladite saumure produite se situe dans la gamme de 100 à 20 000 ppm, de préférence dans la gamme de 200 à 7 000 ppm.

10 7. Le procédé selon l'une quelconque des revendications précédentes, dans lequel la concentration dudit agent de réticulation dans ladite saumure produite se situe dans la gamme de 25 à 5 000 ppm, de préférence dans la gamme de 100 à 2 000 ppm.

15 8. Le procédé selon l'une quelconque des revendications précédentes, dans lequel la concentration dudit ligand complexant dans ladite saumure produite se situe dans la gamme de 25 à 5 000 ppm, de préférence dans la gamme de 100 à 2 000 ppm.

9. Le procédé selon l'une quelconque des revendications précédentes, dans lequel ladite composition est injectée dans un puits d'huile ou de gaz, dans une gamme de température de 26,7 à 93°C, de préférence de 37,8 à 77°C.

20 10. Le procédé selon la revendication 1, dans lequel ladite composition est injectée dans un puits d'huile ou de gaz, dans une gamme de température de 21,1 à 149°C, de préférence de 66 à 121°C, et dans lequel ledit polymère est un copolymère ayant les motifs répétitifs dérivés des monomères choisis parmi l'acrylamide, la N-vinyl-2-pyrrolidone, le 2-acrylamido-2-méthylpropane-sulfonate de sodium, l'acide acrylique et un sel alcalin de l'acide acrylique et leurs combinaisons.

25 11. Une composition appropriée pour le traitement de puits de pétrole comprenant une saumure produite, un polymère soluble dans l'eau, un agent de réticulation, et un ligand complexant, lesdits composants étant définis comme indiqué dans l'une quelconque des revendications 1, 3 à 9 et 10.

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